

FORM PTO-1590 (REV. 5-93)

U.S. DEPARTMENT OF COMMERCE PATENT AND TRADEMARK OFFICE

ATTORNEY'S DOCKET NUMBER

**TRANSMITTAL LETTER TO THE UNITED STATES
DESIGNATED/ELECTED OFFICE (DO/EO/US)
CONCERNING A FILING UNDER 35 U.S.C. 371**

1762.7600

U.S. APPLICATION NO. (If known, see 37 C.F.R. 1.52)

097806469

INTERNATIONAL APPLICATION NO.

INTERNATIONAL FILING DATE

PRIORITY DATE CLAIMED

PCT/FI99/00797

29 September 1999 (09.29.99)

2 October 1998 (10.2.98)

TITLE OF INVENTION

METHOD AND APPARATUS IN A FLUIDIZED BED HEAT EXCHANGER

APPLICANT(S) FOR DO/EO/US


Timo HYPPÄNEN

Applicant herewith submits to the United States Designated/Elected Office (DO/EO/US) the following items and other information:

1. ☒ This is a **FIRST** submission of items concerning a filing under 35 U.S.C. 371.
2. ☐ This is a **SECOND** or **SUBSEQUENT** submission of items concerning a filing under 35 U.S.C. 371.
3. ☒ This is an express request to begin national examination procedures (35 U.S.C. 371(f)) at any time rather than delay examination until the expiration of the application time limit set in 35 U.S.C. 371(b) and PCT Articles 22 and 39(1).
4. ☐ A proper Demand for International Preliminary Examination was made by the 19th month from the earliest claimed priority date.
5. ☒ A copy of the International Application as filed (35 U.S.C. 371(c)(2))
 - a. ☐ is transmitted herewith (required only if not transmitted by the International Bureau).
 - b. ☒ has been transmitted by the International Bureau.
 - c. ☐ is not required, as the application was filed in the United States Receiving Office (RO/US).
- ☐ A translation of the International Application into English (35 U.S.C. 371(c)(2)).
- ☐ Amendments to the claims of the International Application under PCT Article 19 (35 U.S.C. 371(c)(3))
 - a. ☐ are transmitted herewith (required only if not transmitted by the International Bureau).
 - b. ☐ have been transmitted by the International Bureau.
 - c. ☐ have not been made; however, the time limit for making such amendments has NOT expired.
 - d. ☐ have not been made and will not be made.
- ☐ A translation of the amendments to the claims under PCT Article 19 (35 U.S.C. 371(c)(3)).
- ☐ An oath or declaration of the inventor(s) (35 U.S.C. 371(c)(4)).
- ☐ A translation of the annexes to the International Preliminary Examination Report under PCT Article 36 (35 U.S.C. 371(c)(5)).

Items 11. to 16. below concern other document(s) or information included:

11. ☐ An Information Disclosure Statement under 37 CFR 1.97 and 1.98.
12. ☐ An assignment document for recording. A separate cover sheet in compliance with 37 CFR 3.28 and 3.31 is included.
13. ☐ A FIRST preliminary amendment.
☐ A SECOND or SUBSEQUENT preliminary amendment.
14. ☐ A substitute specification.
15. ☐ A change of power of attorney and/or address letter.
16. ☒ Other items or information:
Please examine the application on the basis of substitute claims 1 to 23, attached, which were filed on February 11, 2000, in response to the Written Opinion.

U.S. APPLICATION NO (If known) 09/7806469		INTERNATIONAL APPLICATION NO PCT/FI99/00797		ATTORNEY'S DOCKET NUMBER 1762.7600	
17. <input checked="" type="checkbox"/> The following fees are submitted:				CALCULATIONS	PTO USE ONLY
Basic National Fee (37 CFR 1.492(a)(1)-(5): Search Report has been prepared by the EP or JPO \$860.00 International preliminary examination fee paid to USPTO (37 CFR 1.492(a)(1)) \$690.00 No international preliminary examination fee paid to USPTO (37 CFR 1.492 (a)(1)) but international search fee paid to USPTO (37 CFR 1.492(a)(2)) \$710.00 Neither international preliminary examination fee (37 CFR 1.492(a)(1)) nor international search fee (37 CFR 1.492(a)(2)) paid to USPTO \$1,000.00 International preliminary examination fee paid to USPTO (37 CFR 1.492 (a)(4)) and all claims satisfied provisions of PCT Article 33(1)-(4) \$100.00					
ENTER APPROPRIATE BASIC FEE AMOUNT = \$860.00					
Surcharge of \$130.00 for furnishing the oath or declaration later than <input type="checkbox"/> 20 <input type="checkbox"/> 30 months from the earliest claimed priority date (37 CFR 1.492(e)).				0.00	
Claims	Number Filed	Number Extra	Rate		
Total Claims	23-20 =	3	X \$18.00	\$ 54.00	
Independent Claims	2- 3 =	0	X \$80.00	\$ 0.00	
Multiple dependent claim(s) (if applicable)			+ \$270.00	\$ 0.00	
TOTAL OF ABOVE CALCULATIONS =				\$ 54.00	
Reduction by 1/2 for filing by small entity, if applicable. Verified Small Entity statement must also be filed. (Note 37 CFR 1.9, 1.27, 1.28).				\$	
SUBTOTAL =				\$914.00	
Processing fee of \$130.00 for furnishing the English translation later than <input type="checkbox"/> 20 <input type="checkbox"/> 30 months from the earliest claimed priority date (37 CFR 1.492(f)).				\$	
TOTAL NATIONAL FEE =				\$914.00	
Fee for recording the enclosed assignment (37 CFR 1.21(h)). The assignment must be accompanied by an appropriate cover sheet (37 CFR 3.28, 3.31). \$40.00 per property +				\$	
TOTAL FEES ENCLOSED =				\$914.00	
				Amount to be:	
				refunded	\$
				charged	\$
a. <input checked="" type="checkbox"/> A check in the amount of \$914.00 to cover the above fees is enclosed. b. <input type="checkbox"/> Please charge my Deposit Account No. _____ in the amount of \$ _____ to cover the above fees. A duplicate copy of this sheet is enclosed. c. <input checked="" type="checkbox"/> The Commissioner is hereby authorized to charge any additional fees which may be required, or credit any overpayment to Deposit Account No. 06-1205. A duplicate of this sheet is enclosed.					
NOTE: Where an appropriate time limit under 37 CFR 1.494 or 1.495 has not been met, a petition to revive (37 CFR 1.137(a) or (b)) must be filed and granted to restore the application to pending status.					
SEND ALL CORRESPONDENCE TO:				 SIGNATURE	
FITZPATRICK, CELLA, HARPER & SCINTO 30 Rockefeller Plaza New York, NY 10112-3801				Steven E. Warner NAME	
Date: April 2, 2001				33,326 REGISTRATION NUMBER	

METHOD AND APPARATUS IN A FLUIDIZED BED HEAT EXCHANGER

The present invention relates to a method and an apparatus in a fluidized bed heat exchanger defined in the preambles of the independent claims given below.

The present invention especially relates to a method and an apparatus, by which heat transfer may be adjusted in a fluidized bed heat exchanger, comprising a heat exchange chamber having a bed of solid particles; means for feeding fluidization gas into the heat exchange chamber; heat transfer surfaces in contact with the bed of solid particles; an inlet arranged in the top portion of the heat exchange chamber above the upper surface of the bed of solid particles; and a first outlet for removing solid particles from the heat exchange chamber. The method thus typically comprises the following steps of:

- (a) solid particles are fed through the inlet to the upper surface of the bed of solid particles in the heat exchange chamber;
- (b) the bed of solid particles in the heat exchange chamber is fluidized by fluidization gas;
- (c) heat is transferred by the heat transfer surfaces from the fluidized bed of solid particles; and
- (d) solid particles are removed from the heat exchange chamber through the first outlet.

Fluidized bed heat exchangers are generally used in various pressurized and atmospheric fluidized bed reactor systems, for example, in different combustion and heat transfer processes and chemical and metallurgic processes. Heat typically generated by combustion or other exothermic processes is recovered from solid particles by utilizing heat transfer surfaces. The heat transfer surfaces conduct the recovered heat to a medium, such as water or steam, which transfers the heat out of the reactor.

Heat transfer surfaces may be arranged in different parts of the reactor system, for example in special heat exchange chambers, which may be a part of the reaction chamber, a separate chamber in connection with the
5 reaction chamber, or as in circulating fluidized bed reactors, a part of the circulation system of solid particles.

In many applications of fluidized bed reactors, for
10 example in steam boilers, it is important to be able to adjust the heat transfer continuously and accurately within a wide control range. The reason for the adjustment need may be a changing demand for steam to be produced or a deviation in the fuel quality or in the feed of the fuel
15 or some other abnormality in the system. It may also be necessary to adjust the system to a right operational state. Further requirements for the adjustment of heat transfer in the steam boilers result from the fact that heat is generally recovered at several stages, i.e. in
20 evaporators, superheaters, economizers and reheaters, which may need individual adjustment.

The purpose of the adjustment of heat transfer efficiency in a fluidized bed reactor with respect to the processes
25 is to maintain an optimum operational state in view of emissions and efficiency in the reactor. Often this means that the temperature of the reactor should continue to be constant even in such conditions, in which the heat transfer efficiency and the feed volumes of the fuel
30 fluctuate.

When designing a heat exchange chamber, the most important targets are a simple structure, continuous adjustability
35 within a wide adjustment range and minor space requirements.

106000-8900860

A way to adjust the heat transfer efficiency of a fluidized bed heat exchanger is to change the volume of the fluidized bed material in the heat exchange chamber so that a varying portion of the heat transfer surfaces is covered by solid particles. Such a structure is disclosed, for example, in US patent 4,813,479. In the disclosed arrangement, however, an additional flow channel and an adjustment valve are required, which makes the system more complicated and increases the costs. Further, when changing the height of the bed, part of the heat transfer surfaces may be exposed to considerable erosion.

US patent 5,140,950 discloses an arrangement where the circulation flow of hot solid particles in a circulating fluidized bed reactor is divided by a number of compartments and channels into two separate chambers, only one of which includes heat transfer surfaces. By changing the division ratio of the solid particles flowing through the various chambers, it is possible to vary the heat transfer efficiency of the heat exchanger. The disclosed arrangement is, however, complicated and - in view of space consumption - disadvantageous.

A bubbling fluidized bed is usually maintained in the heat exchange chamber where the speed of the fluidization gas may be, when using bed material with small particle size, for example, 0,1 - 0,5 m/s. The heat transfer efficiency of the fluidized bed heat exchanger may be varied to some extent by changing the speed of the fluidization gas. This is due to the fact that the solid particles move more vividly at high speeds of the fluidization gas than at low speeds, whereby the hot particles spread at high speeds efficiently throughout the whole area of the heat exchange chamber. At high speeds, no separate cooled layers are allowed to be formed in the close proximity of the heat transfer surfaces to decrease the heat transfer, nor will the hot particle flows entering the heat exchanger be

passed directly from the inlet of the heat exchange chamber to the outlet without mixing with the particles in chamber. DE3726643 shows a fluidbed heat exchanger into which bottom particles are fed for contacting heat transfer surfaces before being discharged from its top.

US patent 5,425,412 discloses an arrangement in a circulating fluidized bed reactor, in which the heat exchange chamber includes separate areas for transferring particles and for heat transfer respectively. Heat transfer efficiency is adjusted by changing the moving intensity of the particles close to the heat transfer surfaces and the mixing rate of the material by utilizing the fluidization gas velocities of different areas. By changing the mixing rate of the material the relation between the hot particles newly flown to the chamber and the particles already cooled in the exiting particle flow is varied. In different situations particles may be discharged through an overflow opening in the bed surface and/or through an outlet in the lower portion of the chamber. The adjustment range of the heat transfer efficiency in this kind of a heat exchange chamber may, however, remain rather limited, as in order to avoid agglomeration and overheating of the bed due to possible after-burning the bed of solid particles must be maintained continuously fluidized, whereby the mixing rate is always fairly high. Further, due to the use of a separate transfer area the space utilization is not optimal, since a considerable part of the heat exchange chamber is not in efficient use with respect to the heat transfer.

It is an object of the present invention to provide an improved method and apparatus, in which the above-mentioned problems and defects of the prior art methods and apparatuses are minimized.

It is a more specific object of the invention to provide an improved method and apparatus for easy adjustment of the heat transfer efficiency of a fluidized bed heat exchanger within a wide efficiency range.

- 5 It is still a further object of the present invention to provide a durable and simple, cost-reasonable and space-saving fluidized bed heat exchanger.

- 10 Toward the fulfillment of these objects, the method and apparatus in accordance with the present invention is characterized by what is disclosed below in the characterizing parts of the independent claims.

- The basic idea of the method and apparatus in accordance with the present invention is to be able to restrict the mixing of hot solid particles flowing into the fluidized bed heat exchanger with the bed of solid particles consisting of the solid particles that have come into contact with heat transfer surfaces and/or have otherwise been already cooled. The purpose is thus to be able to
- 15 either partly or even completely prevent the mixing of hot solid particles with the bed of solid particles.
- 20

- The mixing of hot solid particles with the bed of solid particles is restricted by a guiding channel arranged in the fluidized bed heat exchanger to extend from above the surface of the bed of solid particles to the bed of solid particles, and by arranging a first outlet in the area defined by said guiding channel. Hot particles fed through an inlet into the heat exchange chamber may thus be passed
- 25 by the guiding channel to a particular area substantially defined by the guiding channel on the upper surface of the bed of solid particles. Moreover, when the first outlet of the heat exchange chamber is arranged in the area defined by the guiding channel, it is possible to remove hot solid
- 30 particles directly from this area, for example, as an overflow from the upper surface of the solid particle bed or from below the surface through an adjustable outlet or
- 35

5

35

exchanger through the first outlet or through a second outlet arranged in the lower part of the bed.

According to the invention, it is thus possible to
5 restrict the mixing of the cooled solid particles in the bed and the hot solid particles to be removed through the first outlet by passing the hot solid particles to a restricted area on the upper surface of the solid particle bed, from where part of the solid particles may be removed
10 from the heat exchanger in an uncooled state. Thus it is possible to prevent or at least substantially restrict the heat transfer from said specified portion of the solid particles to the solid particle bed and further to the heat transfer surfaces. By utilizing the arrangement
15 according to the present invention, it is possible to decrease the bed temperature and the amount of heat energy to be recovered by the heat transfer surfaces. Thus it is possible, by passing a portion of the particles in an uncooled state out of the heat exchanger, to decrease the
20 smallest possible heat transfer efficiency acquired by each incoming flow of hot particles.

In the arrangement in accordance with the present invention, it is possible to arrange a second outlet in
25 the heat exchange chamber; for example, in the lower portion of the chamber, the solid particle flow through which second outlet can be controlled. Thus it is possible, when producing a high heat transfer efficiency, to let the whole incoming particle flow exit through the
30 second outlet, whereby the means restricting the mixing in the area of the first outlet do not substantially affect to the mixing rate. Thereby the highest possible heat transfer efficiency does not change either.

35 It is typical of the method in accordance with the present invention that the particle flow entering the heat exchanger is passed to the surface of the solid particle

09806459.070601

bed by means extending slightly below the surface to an area defined by said means. The criterion for selecting this restricted area is its connection to the first outlet. The cross-sectional surface area of the restricted area is at the level of the first outlet generally substantially smaller than the average cross-sectional surface area of the particle bed in the heat exchange chamber. The cross-sectional surface area defined by the means is preferably at the level of the lower surface of the first outlet at most 30 %, preferably at most 10 %, of the average cross-sectional area of the particle bed in the heat exchange chamber.

The means restricting the mixing are typically arranged in such a way that they penetrate only over a short distance into the upper part of the bed of solid particles so that the channel or gap formed by them in the bed, where typically no heat transfer surfaces are arranged, would not produce any major waste space in the bed in view of the heat transfer. Thus the means restricting the mixing preferably extend into the bed over a distance which is at most 30 %, most preferably at most 20 %, of the depth of the bed. Typically, the restricting means extend about 10-50 cm, most typically approximately 20-30 cm into the bed.

The invention is applied according to a first preferred embodiment of the present invention to a circulating fluidized bed reactor or boiler, in which the heat exchanger in accordance with the present invention is arranged between the furnace and the return duct of the particle separator in the solids circulation of the reactors, i.e. the tube, through which particles are returned from the particle separator to the furnace of the reactor. The inlet of the heat exchanger is connected to the return duct and the outlet, for example an overflow opening, to the furnace. A first portion of the particles is preferably passed from the return duct in a

substantially uncooled state as an overflow to the furnace. A second portion of the particles is passed to the solids bed in the heat exchange chamber where heat is transferred from the particles to the heat transfer surfaces before the particles are returned to the furnace. The portion to be removed from the circulation as an overflow, possibly varying from 0 to 100 %, varies for example according to the load of the boiler, fuel and volume of the circulation flow.

According to another preferred embodiment, it is possible to apply the invention to a circulating fluidized bed reactor or bubbling bed reactor, in which solids are passed directly to a heat exchanger from a reaction chamber/furnace. In this case the heat exchanger is preferably arranged immediately outside the reaction chamber of the reactor and the heat exchanger and the reaction chamber preferably share a common wall with openings arranged therein forming an inlet for introducing particles into the heat exchange chamber, and an overflow conduit for immediate return of the particles as an overflow to the reaction chamber. These openings may be very close to each other. One and the same opening may in some cases act even in both directions, i.e. alternate in acting as an inlet in one direction and as an overflow opening in another direction. On the other hand, in some cases the upper part of the opening may operate as an inlet and the lower part as an outlet in one and the same opening.

When a fluidized bed heat exchanger is located directly in communication with the reaction chamber of a fluidized bed reactor, often the openings have to be arranged in such a way that material is gathered from a wide area to produce a sufficient material flow. In this case it is particularly important that the incoming material is passed to a small area on the upper surface in the

fluidized bed and it is not allowed to spread throughout this wide surface, where it would inevitably mix with the material which is already in the fluidized bed. By restricting the incoming particle flow to a small area the unnecessary mixing of the material to be removed as an overflow with the rest of the fluidized bed material is restricted as well.

00006469-070904

10 A second outlet for the cooled particles of the heat exchanger is preferably formed at the bottom of the heat exchange chamber, from where particles are passed in a manner known per se, for example, to the furnace. On the other hand, in the above mentioned embodiments the discharge of cooled particles may be arranged to take

15 place through a lifting channel arranged between the heat exchange chamber and the furnace. The bottom of the lifting channel communicates with an outlet in the lower portion of the heat exchange chamber and it preferably shares a common wall with the furnace. Particles are

20 passed from the lifting channel, for example, as an overflow to the furnace.

The arrangement in accordance with the present invention is preferably realized in such a way that the heat

25 exchange chamber has only one continuous fluidized bed of solid particles. Above the fluidized bed the heat exchange chamber is provided with means, e.g. an intermediate plate or a baffle, substantially restricting the spreading of the solid particles introduced through the inlet on the

30 bed of solid particles thus restricting their mixing with the fluidized bed of solid particles as well. When using low fluidization gas velocities, only a first portion of the particles fed to the small area is mainly mixed with the bed of solid particles. The portion corresponds to the

35 amount of particles flowing from the inlet through the heat exchange chamber to the outlet in the lower portion of the heat exchange chamber.

When the demand for heat transfer efficiency is small, the particle flow flowing through the heat exchanger, in other words the particle flow coming in and flowing out, is allowed to pass only through a restricted area of the upper surface of the solid particle bed, whereby the solid particle exchange between the exiting flow and the bed of solid particles is small. Particles, which have not yet had time to settle in the area of efficient mixing of the bed and thus not yet released any heat to the solids bed, may be readily removed as an overflow from the thick layer of hot particles formed in a small area.

In the arrangement in accordance with the invention, only a material flow necessary for the heat transfer is mixed with the bed of solid particles in the heat exchange chamber, the excess returning in a hot state from the upper surface of the bed to the reaction chamber and thus without substantially mixing with the fluidized bed in the heat exchange chamber.

In a heat exchange chamber in accordance with the invention, an efficient and wide-ranging adjustment of heat transfer may be realized simply by adjusting the velocity of the fluidization gas, and if necessary, by further adjusting the discharge of solid particles through a second outlet. By intensifying the particle flow through the second outlet, the amount of uncooled particles flowing through the first outlet is decreased and the amount of particles coming into communication with the heat transfer surfaces is increased. Respectively, by decreasing the particle flow through the second outlet, the immediate discharge of hot particles from the heat exchanger through the overflow opening is increased.

In the arrangement in accordance with the invention, it is not necessary to divide the heat exchanger by intermediate

walls into separate beds of solid particles provided with an individual fluidization.

The invention is described below more closely with reference to the accompanying drawings, in which

- Fig. 1 schematically illustrates a vertical, cross-sectional view of a fluidized bed heat exchanger in accordance with the invention;
- 10 Fig. 2 schematically illustrates a cross-sectional view of a circulating fluidized bed boiler provided with a heat exchanger in accordance with the first embodiment of the invention;
- 15 Fig. 3 schematically illustrates an enlargement of Fig. 2 at the overflow opening and a first exemplary embodiment of the invention, in which the heat exchanger in accordance with the invention is connected to the return duct in the separator of the circulating fluidized bed boiler; and
- 20 Fig. 4 schematically illustrates a cross-sectional view of a heat exchanger in accordance with a second embodiment of the invention.

Fig. 1 schematically illustrates a simple heat exchanger 10, in the heat exchange chamber 12 of which a slow fluidized bed 14 comprising hot solid particles is maintained by feeding fluidization gas into it from a wind box 16 through a grid 18. Heat transfer surfaces 30 are arranged in the fluidized bed for the recovery of heat from the fluidized bed. The flow of the incoming fluidization gas from the wind box through the grid 18 may be adjusted by a valve 22, for example, to control the quantity of heat transferring to the heat transfer surfaces.

35

The top portion of the heat exchange chamber 12 above the fluidized bed 14 is provided with an inlet 24, from which

hot solid particles flow through a guiding channel 26 on the surface 28 of the fluidized bed 14.

Heat is recovered from the hot particles entering the fluidized bed in the heat exchange chamber 12 by transferring the heat energy of the hot solid particles to a medium, usually steam or water, contained in the heat transfer surfaces 30. The top portion of the heat exchange chamber 12, immediately below the surface 28 of the fluidized bed 14 is provided with an outlet 34 in the wall 32 of the heat exchange chamber, through which solid particles are removed from the heat exchange chamber to the adjacent space 36 typically being, for example, a furnace. The outlet 34 is preferably a so-called gill-seal type block provided with a gas lock disclosed in the Finnish patent application FI 952193 of the applicant. A separate feed for fluidization air possibly required by the "gill-seal" type outlet is not illustrated in Fig. 1. The outlet may also be another kind of a conduit or an opening, the opening extent and flow-through of which is adjustable.

Continuous fluidization must be often maintained in the particle bed 14 to prevent agglomeration of the bed and local overheating. To prevent the hot solid particles flowing through the inlet 24 to the upper surface of the bed from mixing rapidly with the bed 14 due to fluidization, a baffle or an intermediate wall 38 considerably restricting said mixing is arranged in the heat exchange chamber. The intermediate wall 38 forms one of the guiding channel 26 walls.

The intermediate wall 38 arranged in the top portion of heat exchange chamber 12 between the inlet 24 and the upper surface 28 of the fluidized bed 14 passes the hot solid particles through the inlet 24 toward an area 28' on the upper surface 28 of the fluidized bed defined by the

0306465-070001

intermediate wall 38 and the wall 32 of the heat exchange chamber. The intermediate wall 38 and the wall 32 of the heat exchange chamber 12 form a guiding channel 26 extending over and partly into the fluidized bed. The intermediate wall 38 extends lower than the lower edge of the outlet and at the guiding channel prevents the free movement of the material entering the heat exchange chamber within the surface 28 area of the fluidized bed 14. On the other hand, in order to avoid a major waste space, the guiding channel 26 formed by the wall 32 of the heat exchange chamber 12 and the intermediate wall 38 may not be too long. In the example of Fig. 1, the length of the guiding channel portion in the solid particle bed is less than 30 % of the depth of the bed. The intermediate wall 38 extends over a distance "h" into the fluidized bed, the distance typically being 10-50 cm.

The cross-sectional area A_1 of the area 28' restricted by the guiding channel from the surface 28 of the fluidized bed is at most 30 % of the average cross-sectional area A_2 of the fluidized bed. Thus the solid particles flowing through the inlet 24 to the fluidized bed, which particles in a heat exchange chamber not equipped with intermediate walls would spread throughout the entire upper surface of the fluidized bed, are packed within the area defined by the guiding channel 26 in the arrangement in accordance with the invention.

When low heat transfer efficiency is desired using a heat exchange chamber in accordance with Fig. 1, a fluidization gas velocity as low as possible has to be used, i.e. a so-called minimum fluidization, by which solid particles still move relative to each other. If the intermediate wall 38 did not exist, the hot solid particles entering through the inlet 24 would be allowed to spread throughout the entire surface 28 of the solid particle bed, whereby they would efficiently mix with the bed 14 of solid

particles regardless of the low velocity of the fluidization gas. In the arrangement of Fig. 1 in accordance with the invention the intermediate wall 38 passes the hot solid particles entering through the inlet 5 to the restricted area 28' on the upper surface of the solid particle bed. When using a low fluidization gas velocity, the mixing of the hot solid particles forced to the restricted bed area 28' is slow or practically no mixing takes place at all. As the outlet 34 is in the area 10 of the solid particle bed defined by the guiding channel 26, hot solid particles newly entered the heat exchange chamber mainly through the inlet 24 and not yet being mixed with the particles in the bed, are discharged from the heat exchange chamber 12 through the outlet 34. Since 15 no substantial quantities of hot particles enter the bed, the temperature of the bed 14 remains substantially low and the heat transfer minor.

On the other hand, if high heat transfer efficiency is 20 desired using a heat exchange chamber in accordance with Fig. 1, a high fluidization gas velocity has to be used. In this case the entire solid particle bed is in a very intensive inner movement, whereby also the particles entering through the inlet 24 mix rapidly with the solid 25 particle bed 14 in the heat exchange chamber regardless of the intermediate wall 38. Thus almost the entire bed of solid particles, including most of the bed portion defined by the guiding channel 26, is substantially at the same temperature and its heat transfer efficiency is maximal.

30 According to the above description, the intermediate wall 38 diminishes the lowest possible heat transfer efficiency available in the heat exchange chamber 12, but it does not substantially affect the highest possible heat transfer 35 efficiency available. Thus, the intermediate wall restricting the mixing makes the adjustment range of the heat transfer in the heat exchange chamber considerably

wider, which is of great importance in many applications of heat exchange chambers.

Fig. 2 illustrates a heat exchanger connected to a circulating fluidized bed boiler in accordance with the invention. In Fig. 2 the same reference numbers are used, as in Fig.1, wherever possible.

Fig. 2 thus illustrates a circulating fluidized bed boiler 40, comprising a furnace 36, a particle separator 42, a gas outlet pipe 44, and a return duct 46 for solid particles including a gas lock 48. A fast fluidized bed comprising hot solid particles is maintained in the furnace 36 by feeding fluidization gas to the bed from a wind box in a manner known per se, so that solid particles are entrained with the exit gas through an opening in the top portion of the furnace to the particle separator 42. The particle separator separates most of the hot solid particles from the exit gas and the separated solid particles are returned through the return duct 46 arranged in the lower portion of the separator to the furnace 36.

In communication with the return duct 46 is arranged a heat exchanger 10 in accordance with the invention, in the heat exchange chamber 12 of which a slow fluidized bed 14 consisting of hot solid particles is maintained by feeding fluidization gas from a wind box 16 through a grid 18. The fluidized bed is provided with heat transfer surfaces 30 to recover heat from the fluidized bed.

The top portion of the chamber 12 above the fluidized bed is provided - although not illustrated in Fig. 1 - with an opening or a duct, through which the fluidization air is allowed to flow from the heat exchange chamber to the furnace. Moreover, the top portion of heat exchange chamber 12 above the fluidized bed 14 is provided - as can be seen more clearly in Fig. 3 - with an inlet 24

5 The bottom of the heat exchange chamber 12 is provided with an outlet 50, through which solid particles can be removed from the heat exchange chamber and passed along a duct 52 to the furnace 36. The volume of the solid particle flow to be removed through the outlet 50 can be
10 adjusted by using a valve 56 to change the volume of the fluidization and blast air to be fed through pipes 54 to the duct 52. When the volume of the solid particle flow to be removed through the outlet 50 is less than that of the hot solid particle flow entering the heat exchange
15 chamber, the excess of the solid particles exits from the heat exchange chamber 12 directly from the upper surface of the bed 14 through an overflow opening 58 arranged in a wall 60 of the heat exchange chamber below the inlet 24. The wall 60 is at the inlet 24 shared by the heat exchange
20 chamber 12 and the furnace 36. The heat exchange chamber and the furnace may also be completely separate from each other not sharing a wall or wall part. In the case of Fig. 2 only the uppermost part of the wall of the heat exchange chamber is shared with the furnace. If the chambers are
25 completely separate, it is possible to arrange a duct or a pipe between them, through which the solid particles exiting from the heat exchange chamber, can be returned to the furnace.

30 The intermediate wall 62 restricting the mixing arranged in the top portion of the heat exchange chamber 12 between the inlet 24 and the fluidized bed 14, passes the hot solid particles from the inlet toward an area 28' of the upper surface 28 of the fluidized bed 14 defined by the
35 intermediate wall 62 and the wall 60 of the heat exchange chamber. The intermediate wall 62 and the wall 60 of the heat exchange chamber 12 form a guiding channel 66 above

the fluidized bed and partially penetrating into the fluidized bed. The intermediate wall 62 extends lower than the lower edge of the overflow opening 58 and at the guiding channel prevents the free movement of the incoming material on the surface of fluidized bed 14. On the other hand, in order to avoid a major waste space, the guiding channel 66 formed by the wall 60 of the heat exchange chamber and the intermediate wall 62 may not be too long. In the example disclosed in Fig. 1, the length of the guiding channel 66 is less than 20 % of the depth of the bed 14. The intermediate wall 62 extends over a distance "h" below the upper surface of the fluidized bed, the distance typically being 0-50 cm. An area A₁ restricted by the guiding channel from the fluidized bed is at most 30 % of the average cross-sectional area A of the fluidized bed.

Part of the hot solid particles is allowed to flow from the channel 66 through the overflow opening 58 to the furnace 36 without mixing with the solid particles in the lower portion of the guiding channel, or mixing only with a substantially small amount of cooled solid particles in the area of the guiding channel. A controllable portion of the hot solid particles flow in an uncooled state directly to the furnace. In order to have as minimal mixing of the particles in the bed 14 with the hot particles exiting through the overflow opening 58 as possible, the overflow opening is located very close to the inlet in the arrangement of Fig. 2.

30

Since the particles exiting through the outlet 50 come much more into contact with the heat transfer surfaces 30 than the particles exiting through the overflow opening 58, the heat transfer efficiency of the heat exchanger 10 may be adjusted by changing the ratio of the particle flows exiting through the outlet 50 and the overflow opening 58 respectively. When the fluidization velocity of

the bed 14 is constant, the heat transfer efficiency is at its highest when all particles exit through the outlet 50 and at its lowest when all particles exit through the overflow opening 58.

5

In a typical case, the lowest heat transfer efficiency achieved having the discharge from the heat exchange chamber only through the overflow 58 would be in the order of 60-80 % of the maximum efficiency, if no intermediate wall 62 were provided. Owing to the intermediate wall 62, the exchange of particles in the bed 14 by using minimum efficiency is insignificant and the minimum efficiency may be as low as only 20 % of the maximum efficiency. This widening of the adjustment range is of great importance when various kind of adjustment of the heat exchanger 10 is required.

The guiding channel 66 and the overflow opening restricting the inlet flow of the hot solid particles are formed preferably in a point, from where the solid particles may be returned in a simple manner to the furnace. In the case of Fig. 2 showing the cross-section at the overflow opening, the overflow opening is intended to be arranged in the middle of the wall 60 of the heat exchanger. If desired, the guiding channel and the overflow opening may be arranged in either side of the heat exchanger or in some other suitable place, or there could be more than just one overflow opening arranged at a distance from each other.

20
25
30

In the arrangement of Fig. 4 the same reference numbers are used as in Figs. 1, 2, and 3, wherever possible.

Fig. 4 discloses a heat exchange chamber 12 of a heat exchanger 10, said heat exchange chamber being arranged outside a wall 60 in a furnace 36 of a fluidized bed reactor, circulating fluidized bed reactor or bubbling

09505463-070001

fluidized bed reactor. A bed 14 of solid particles is fluidized by fluidization gas blown through a grid 72 from a wind box 70 and heat energy is recovered from the bed of heat transfer surfaces 30.

5

The flow of solid particles is passed through an inlet 74 to the upper surface 28 of the solid particle bed 14. The hot solid particles entering through the inlet 74 are passed by a guiding channel 78 formed by an intermediate wall 76 toward the fluidized bed, to a restricted area 28' on its upper surface. Hot solid particles exit through an overflow opening 80 provided in the area defined by the intermediate wall, the upper surface of the fluidized bed being flush with the lower edge of the overflow opening or higher.

A vertical lifting channel 82 is formed between the furnace 36 and the actual heat exchange chamber 12 of the heat exchanger 10. The heat exchange chamber 12 and the lifting channel 82 are in communication with each other through an outlet 84 in their respective bottom parts. The top portion of the lifting channel is provided with a second overflow opening 88 in the wall 86 shared by the lifting channel and the furnace for the removal of solid particles as an overflow from the lifting channel to the furnace.

The ratio of the volume of the solid particle flow "V" exiting through the second overflow opening 88 of the lifting channel 82 to that of the flow "v" exiting through the overflow opening 80 arranged in the top portion of the heat exchange chamber can be adjusted by a valve 90 regulating the volume of the flow exiting through the channel 82, i.e. the fluidization. Due to the intermediate wall 76 preventing the mixing, the flow exiting through the overflow opening 80 does not substantially mix with the particles in the fluidized bed 14. The solid particle

flow through the overflow opening 80 consists of hot solid particles newly flown in through the inlet 74.

In the above the invention has been described in connection with embodiments that are presently considered as the most preferable. However, it must be understood that the invention is not limited to these embodiments only, but it also covers a number of other arrangements within the scope of invention determined by the patent claims below.

Thus, it must be understood that the heat exchanger may also be arranged in some other way into communication with the reaction chamber, e.g. inside the reaction chamber. Thus the particle inlet may be arranged to operate in communication with the inner material circulation of the reaction chamber.

Furthermore, the number of inlets and outlets, the location and structure thereof may deviate from what is disclosed herein, and the structure and shape of the means restricting the mixing of particles may as well deviate from the embodiments disclosed herein.

Claims

1. Method of controlling heat transfer in a fluidized bed heat exchanger (10), having a heat exchange chamber (12) with a bed (14) of solid particles therein, the method comprising the following steps:
- (a) feeding solid particles through an inlet (24, 74) in the top portion of the heat exchange chamber to the upper surface (28) of the bed of solid particles therein, thereby passing the solid particles by a guiding channel (26, 66, 78) to an area (28'), defined by said guiding channel, of said upper surface;
 - (b) fluidizing the bed of solid particles in the heat exchange chamber by fluidization gas;
 - (c) transferring heat by heat transfer surfaces (30) away from the fluidized bed of solid particles; and
 - (d) removing solid particles from the heat exchange chamber,
- characterized by
- in step (d) removing solid particles from the heat exchange chamber through a first outlet (34, 58, 80) formed in the area of the guiding channel.
2. A method according to claim 1, characterized by feeding solid particles to the heat exchange chamber to an area (28') of the upper surface of the bed of solid particles, the cross-sectional surface area of which is at most 30 %, preferably at most 10%, of the average cross-sectional area of the bed of solid particles.
3. A method according to claim 1, characterized by restricting with an intermediate wall (38, 62, 76), which forms one wall of the guiding channel and which is inserted in the bed of solid particles, the horizontal

movement of solid particles between the guiding channel and the rest of the of the solid particle bed.

4. A method according to claim 1, characterized by
5 removing solid particles from the heat exchanger by overflow from the surface of the bed of solid particles in the heat exchange chamber.
5. A method according to claim 1, characterized by
10 removing solid particles from the heat exchanger from below the surface of the bed of solid particles in the heat exchange chamber through a first adjustable outlet.
6. A method according to claim 1, characterized by
15 removing further solid particles from the heat exchanger through a second outlet (50, 84) in the lower portion of the heat exchange chamber.
7. A method according to claim 6, characterized by
20 adjusting the heat exchange in the heat exchanger by regulating the amount of solid particles passing through the second outlet.
8. A method according to claim 1, for controlling heat
25 transfer in a fluidized bed heat exchanger in a circulating fluidized bed reactor, the heat exchanger having the inlet (24) connected to a return duct (46) of a particle separator (42) of the circulating fluidized bed reactor and the outlet (58) to a furnace (36) of the
30 circulating fluidized bed reactor, characterized by returning solid particles flowing from the return duct (46) to the heat exchange chamber (12) directly from the area (28') defined by the guiding channel (66) to the furnace (36) of the circulating fluidized bed reactor.
- 35 9. A fluidized bed heat exchanger (10) comprising

- a heat exchange chamber (12) having a bed (14) of solid particles therein;
- means (16,18) for feeding fluidization gas into the heat exchange chamber for fluidizing the bed of solid particles therein;
- heat transfer surfaces (30) in contact with the bed of solid particles in the heat exchange chamber;
- an inlet (24, 74) arranged in the top portion of the heat exchange chamber, for feeding solid particles to the heat exchange chamber;
- a guiding channel (26, 66, 78) extending from above the upper surface (28) of the bed of solid particles at least to the surface (28) of said bed of solid particles, for guiding solid particles from said inlet (24, 74) to an area (28') defined by the guiding channel on the upper surface of the bed of solid particles and
- a first outlet (34, 58, 80), for removing solid particles from the heat exchange chamber, characterized in
- the first outlet (34, 58, 80) being formed in the area of the guiding channel (26, 66, 78), for the removal of solid particles from the bed of solid particles in the area defined by the guiding channel.
10. A fluidized bed heat exchanger according to claim 9, characterized by the area (28') defined by the guiding channel on the upper surface of the bed of solid particles being at most 30 %, preferably at the most 10 %, of the average cross-sectional area of the bed of solid particles.
11. A fluidized bed heat exchanger according to claim 9, characterized by the area (28') defined by the guiding channel on the upper surface of the solid particle bed being abutted on a first wall (32) of the heat exchange chamber.

12. A fluidized bed heat exchanger according to claim 11, characterized by the first outlet (58, 80) comprising an overflow opening arranged flush with the surface of the bed of solid particles.

5

13. A fluidized bed heat exchanger according to claim 11, characterized by the first outlet (34) comprising an adjustable outlet arranged below the surface of the bed of solid particles.

10

14. A fluidized bed heat exchanger according to claim 9, characterized by a second outlet (50, 84) being arranged in the heat exchange chamber.

15

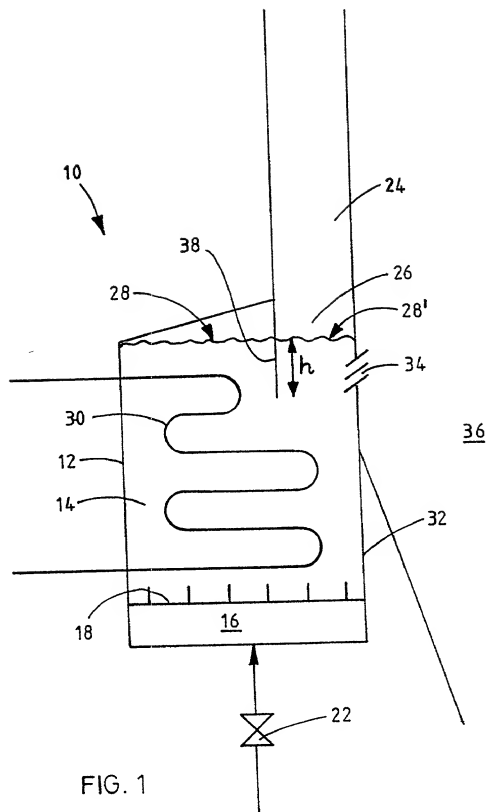
15. A fluidized bed heat exchanger according to claim 14, characterized by the second outlet (50) being arranged in the bottom of the heat exchange chamber.

20

16. A fluidized bed heat exchanger according to claim 14, characterized in
- the second outlet (84) being arranged between the heat exchange chamber and a lifting channel (82) formed adjacent to the heat exchange chamber and
- an overflow opening (88) being arranged in the top
25 portion of the lifting channel for the removal of solid particles from the lifting channel.

17. A fluidized bed heat exchanger according to claim 9, characterized by the guiding channel (26, 66, 78) being
30 abutted on the wall (32) of the heat exchange chamber and on an intermediate wall (38, 62, 76) arranged in the heat exchange chamber, the intermediate wall (38, 62, 76) extending from above the surface (28) of the solid particle bed at least to the surface of the bed of solid
35 particles.

18. A fluidized bed heat exchanger according to claim 17, characterized by the intermediate wall (38, 62, 76) extending from the surface of the bed of solid particles about 10 - 50 cm, preferably about 20 - 30 cm, below the surface.
19. A fluidized bed heat exchanger according to claim 17, characterized by the intermediate wall (38, 62, 76) penetrating into the solid particle bed at most 20 % of the depth of the bed.
20. A fluidized bed heat exchanger according to claim 9, characterized in a second outlet (50) being spaced apart from the vertical projection of the guiding channel in the bottom of the heat exchange chamber.
21. A fluidized bed heat exchanger according to claim 9, characterized in the heat exchange chamber being provided with a continuous bed of solid particles having a continuous fluidization.
22. A circulating fluidized bed reactor having a fluidized bed heat exchanger according to claim 9, characterized by the inlet (24) of the fluidized bed heat exchanger being connected to a return duct (46) of a particle separator (42) of the circulating fluidized bed reactor and the first outlet (34,58) to a furnace (36) of the circulating fluidized bed reactor.
23. A fluidized bed reactor having a fluidized bed heat exchanger according to claim 9, characterized by the inlet (74) of the fluidized bed heat exchanger being connected directly to the furnace (36) of the fluidized bed reactor.



09/806469

2/3

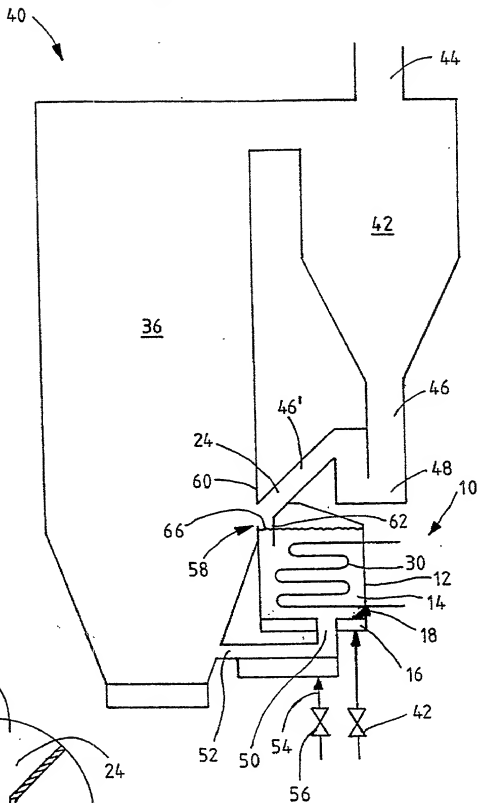


FIG. 2

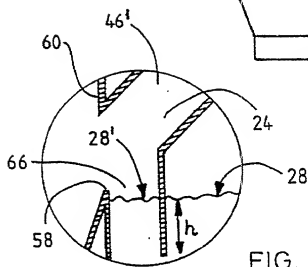


FIG. 3

AMENDED SHEET

09806469.070901

09/806469

3/3

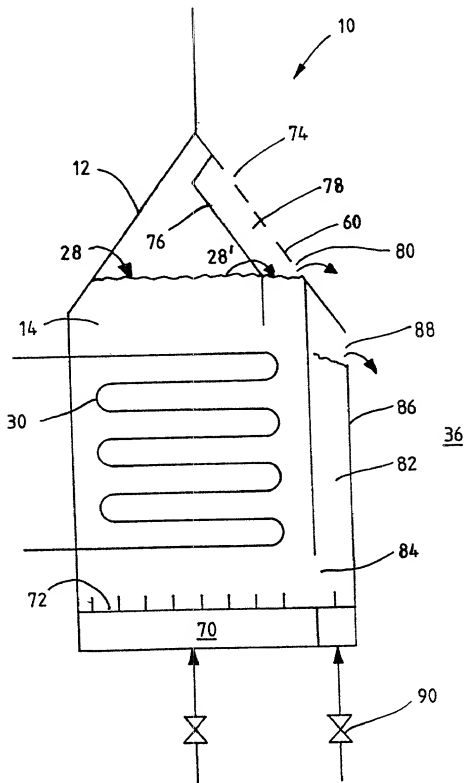


FIG. 4



COMBINED DECLARATION AND POWER OF ATTORNEY
FOR PATENT APPLICATION
(Page 1)

As the below named inventor, I hereby declare that:

My residence, post office address and citizenship are as stated below next to my name;

I believe I am the original inventor of the subject matter which is claimed and for which a patent is sought on the invention entitled METHOD AND APPARATUS IN A FLUIDIZED BED HEAT EXCHANGER, the specification of which was filed on _____, 2001, as United States Application No. (not yet assigned), which is based on PCT International Application No. PCT/FI99/00797 and was amended on _____ (if applicable).

I hereby state that I have reviewed and understand the contents of the above-identified specification, including the claims, as amended by any amendment referred to above.

I acknowledge the duty to disclose information which is material to patentability as defined in 37 CFR §1.56.

I hereby claim foreign priority benefits under 35 U.S.C. §119(a)-(d) or §365(b), of any foreign application(s) for patent or inventor's certificate, or § 365(a) of any PCT international application which designates at least one country other than the United States, listed below and have also identified below any foreign application for patent or inventor's certificate, or PCT international application having a filing date before that of the application on which priority is claimed:

Country	Application No.	Filed (Day/Mo./Yr.)	(Yes/No) Priority Claimed
Finland	FI-982135	2/October/1998	Yes
PCT	FI99/00797	29/September/1999	Yes

I hereby claim the benefit under 35 U.S.C. § 120 of any United States application(s), or § 365(c) of any PCT international application designating the United States, listed below and, insofar as the subject matter of each of the claims of this application is not disclosed in the prior United States or PCT international application in the manner provided by the first paragraph of 35 U.S.C. § 112, I acknowledge the duty to disclose information which is material to patentability as defined in 37 C.F.R. § 1.56 which became available between the filing date of the prior application and the national or PCT international filing date of this application.

Application No.	Filed (Day/Mo./Yr.)	Status (Patented, Pending, Abandoned)
-----------------	---------------------	--

I hereby appoint the practitioners associated with the firm and Customer Number provided below to prosecute this application and to transact all business in the Patent and Trademark Office connected therewith, and direct that all correspondence be addressed to the address associated with that Customer Number:

FITZPATRICK, CELLA, HARPER & SCINTO
Customer Number: 05514

I hereby declare that all statements made herein of my own knowledge are true and that all statements made on information and belief are believed to be true; and further that these statements were made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment, or both, under Section 1001 of Title 18 of the United States Code and that such willful false statements may jeopardize the validity of the application or any patent issued thereon.

Full Name of Sole Inventor Timo HYPÄNEN

Inventor's signature [Signature]

Date April 12, 2001

Citizen/Subject of Finland

Residence Siikakoskenpolku 10, FIN-48710 Karhula, Finland FIX

Post Office Address c/o Foster Wheeler Energia Oy, Nuijamiestentie 3,
FIN-00400, Helsinki, Finland